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Description

This invention relates to improved amphoteric starch derivatives containing both cationic substituent groups and anionic phosphate groups. The invention also relates to a process for preparing these amphoteric starches and their use as wet-end additives showing improved drainage in the manufacture of paper.

As used herein, the term "paper" includes sheet-like masses and molded products made from fibrous cellulosic material, which may be derived from natural sources as well as from synthetics such as polyamides, polyesters and polyacrylic resins, as well as from mineral fibers such as asbestos and glass. Also included are papers made from combinations in cellulosic and synthetic materials. Paperboard is also included, within the broad term "paper".

It has been known to add various materials, including starch, to the pulp, or stock, during the papermaking process, prior to the formation of the sheet. The purpose of such additives has been mainly to bind the individual fibers to one another, thus aiding the formation of a stronger paper.

In the case of those papers which contain added pigments, such for example as titanium dioxide, it has been known to add materials to the pulp, or stock, for the specific purpose of retaining a greater proportion of such pigments in the paper (rather than have them drain off in the water that is removed during the formation of the sheet). Such additives are often referred to as "pigment retention agents".

Anionic and cationic starches as well as amphoteric starches have long been used as additives in papermaking for their contributions to strength and pigment retention in the paper. See, for example, US-A-3,459,632 and US-A-3,562,103.

In recent years, in an effort directed to improving machine speeds, reducing drying time and generally improving costs, paper makers have begun to focus on the efficiency of water removal or drainage during the sheet-forming process. See, for example, the article by K. W. Britt in TAPPI Journal, Jan 1984, p 102-103 and the article by A. M. Springer et al., TAPPI Journal, Feb 1984 p 104-108. In ordinary papermaking operations employing Fourdrinier type machines, the pulp furnish or stock is fed from a headbox onto a wire screen where the web is first formed. Water is drained from the stock by gravity and by vacuum suction, and then by pressing. Drainage efficiency is affected by a number of factors including the composition and pH of the furnish. It can be understood that even minor improvements in drainage efficiency can have significant savings in the cost of producing large volumes of paper which are produced.

While starch additives of the prior art used for strength and pigment retention also show some favorable effects on improving drainage performance, we have found that the use of the amphoteric starch additives described hereinbelow, meeting specified criteria particularly with respect to bound phosphorus, surprisingly provide improved drainage with no untoward effects on strength or pigment retention. Testing results have shown that the amphoteric starch additives of the present invention will typically improve drainage by 20-30% over a representative commercially used amphoteric starch additive.

Accordingly, one object of the invention is to provide a process for preparing amphoteric starches meeting criteria with respect to molecular weight, bound phosphorus, cationic degree of substitution, and the ratio of anionic to cationic groups.

Another object of the invention is to provide an improved amphoteric starch containing cationic groups and anionic phosphate groups meeting criteria with respect to molecular weight, bound phosphorus, cationic D.S. (degree of substitution), and the ratio of anionic to cationic groups.

A further object of the invention is to provide an amphoteric starch for use as a wet-end additive showing improved drainage in the manufacture of paper and increasing the strength and pigment retention of paper products.

The above objects are solved by a process for preparing an amphoteric starch derivative which comprises:

- (a) providing an aqueous slurry of a starch derivative containing tertiary amino or quaternary ammonium cationic substituent groups having a degree of substitution of from 0.010 to 0.080,
- (b) adjusting the pH level of the slurry to pH 5.5-8.5,
- (c) adding to the aqueous starch slurry a phosphate salt selected from the group consisting of tripolyphosphate, hexametaphosphate, and pyrophosphate alkali metal salts, while maintaining the pH level at 5.5-8.5,
- (d) filtering the slurry,
- (e) drying the resultant cake to a moisture of 9.0 % by weight or below,
- (f) heat reacting the dried starch at a temperature of 110-140 °C for a period of 0.1 to 4.0 hours, and
- (g) recovering the amphoteric starch derivative, wherein the resultant starch derivative has a bound

phosphorus content of at least 0.12 %, a viscosity of at least 800 mPa.s (800 cps), and a ratio of anionic to cationic groups of from 0.12 to 0.55.

The novel additives of our invention are starch derivatives containing cationic groups, together with a controlled amount of anionic phosphate groups. The derivatives are prepared by treating a suitable starch to provide it with tertiary amino or quaternary ammonium cationic groups and thereafter treating it with a selected inorganic phosphate reagent. In reacting the starch with the cationic and phosphate reagents, conditions must be employed to avoid crosslinking and also avoid degradation of the starch so that, in effect, there is a preservation of molecular weight. The molecular weight of the starch derivative can be conveniently correlated to its viscosity, as measured on a starch dispersion (2.0% by weight, dry basis) in potassium hydroxide (KOH) using a Brookfield Viscometer at 10 rpm. The starch derivative herein must possess a viscosity of at least 800 mPa.s (800 cps), and preferably above 1000 mPa.s (1,000 cps). Viscosity measurements below about 800 mPa.s (800 cps) are indicative of a detrimental degradation of the starch which renders it unsuitable for use herein. The starch derivative must also contain at least a specified minimum amount of bound phosphorus. We have found that to obtain improved drainage, it is necessary that the starch contain at least 0.12% of bound phosphorus and preferably about 0.14%. If other criteria are met, it appears that higher concentrations of phosphorus in the derivative lead to improved drainage performance.

In order to be most effective as an additive in the process of our invention, the selected starch derivative should have a ratio of anionic, i.e., phosphate groups to cationic groups, (A/C) ratio, within the range of from about 0.12 to 0.55 moles of anionic groups per mole of cationic group. Furthermore, the starch derivatives should be substituted with cationic groups to such an extent that their degree of substitution (D.S.) i.e., the average number of cationic groups per anhydroglucose unit of the starch molecule ranges from 0.010 to 0.080.

Suitable starches which may be employed in the process include, for example, starches derived from corn, waxy maize, potato, tapioca, rice, sago, sorghum and wheat. Also included are starches which have higher amylose contents, e.g., 35% or more by weight of amylose. Preferred starches useful herein are waxy maize, corn, tapioca, potato and blends of these starches. It is to be noted that the starch base employed herein is usually in its granular form, i.e., it should be any amyloseous material which has not lost its granular polarization crosses and is capable of swelling. However, it is possible in the practice of this invention to employ a granular starch of which a small portion has been partially swelled by any known means or homogenized by subjecting it to shear.

As the cationic substituent in our starch additive, we prefer tertiary amino or quaternary ammonium groups. However, other cationic groups are operable as, for example, primary and secondary amine groups, sulfonium and phosphonium groups. The preparation of aminoalkyl ethers of starch, wherein the starch derivative contains tertiary amine groups, is described in US-A-2,813,093. Similarly, sulfonium and phosphonium derivatives of starch are described in US-A-2,989,520 and US-A-3,077,469 respectively.

It is known that quaternary amine groups may be introduced into the starch molecule either by suitable treatment of the tertiary aminoalkyl ether of starch, as described for example in US-A-2,813,093, or quaternary groups may be introduced directly into the starch molecule as, for example, by treatment with the reaction product of an epihalohydrin and a tertiary amine or tertiary amine salt.

Other suitable cationic starch derivatives will be apparent to the practitioner, it being remembered that our process may employ any starch derivative which contains a cationic (i.e. electrically positively charged) moiety in the starch molecule. Preferred starches herein for further substitution with phosphate groups are the diethylaminoethyl ether or 2-hydroxypropyl trimethylammonium ether of waxy maize, corn, tapioca and potato starch.

As stated, the starch derivative, to be suitable as an additive to paper pulp in the process of our invention, must also contain a controlled amount of anionic phosphate groups.

Techniques for phosphorylating a starch base are known to those skilled in the art. Thus, US-A-2,824,870; US-A-2,884,412 and US-A-2,961,440 disclose various phosphorylation techniques consisting, essentially, of heat reacting starch impregnated with a phosphate salt of an alkali metal, within a prescribed pH range. Above-mentioned US-A-3,562,103 directed to starches containing quaternary and anionic phosphate groups discloses a preferred method of phosphating a starch which comprises forming an aqueous starch slurry at room temperature and adding a suitable concentration of phosphate reagent. Preferably the pH is adjusted to between 4 and 6, although it is stated that a range of 4 to 11.5 may be used. The starch is filtered without washing and adjusted to a moisture level of about 20% or below, preferably from 5 to 20% by weight at a temperature of less than about 70°C. The starch-phosphate composition is then roasted at a temperature of 100-160°C until the product has the desired level of anionic phosphate groups.

In US-A-4,166,173, which disclosure is incorporated herein by reference, starch is phosphorylated by an

improved pollution-free process which involves forming a concentrated reagent solution of alkali metal tripolyphosphate salt and impregnating therewith a starch cake containing no more than 45% by weight of moisture. Drying and heat reacting the thus impregnated starch provides the phosphorylated starch. In preparing the concentrated reagent solution during addition of the tripolyphosphate salt to the water, one or
5 more acids are added to control the pH at between 2.8 and 5.0.

For the purpose of this invention, the phosphorylation may be carried out by any known techniques provided that the heating of the starch and phosphate salt is carried out at a pH between 5.5 and 8.5, and preferably 6.0 to 8.5, and is limited to reactions of starch with sodium or potassium tripolyphosphate, sodium or potassium hexametaphosphate and sodium or potassium pyrophosphate salts yielding orthophosphate mono-ester groups, i.e., mono-starch phosphates. Other alkali metal salts may be used in place of sodium or potassium which are preferred as the phosphating reagent.
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Thus, in carrying out phosphorylations employing an aqueous starch slurry, the pH of the starch slurry containing the phosphorylating reagent is adjusted to 5.5 to 8.5. Use of pH levels below about 5.5 will result in a degraded starch while use of pH levels above about 8.5 may produce undesirable cross-linking. If
15 phosphorylation is to be carried out by spraying the reagent, a starch slurry is ordinarily prepared and adjusted to be within the designated pH range and is then filtered. The reagent is sprayed onto the pH adjusted starch cake. The practitioner will recognize that it is also possible to prepare the filter cake at a slightly alkaline pH and impregnate it with an acidic solution of phosphate reagent such that the final pH of the starch-phosphate reagent mixture is within the defined pH range. The specific reagent used may require
20 adjustments of pH levels. For example, sodium tripolyphosphate (STP) has limited solubility in water (14.5 g/cc at 25 °C). In order to achieve higher solids solutions, the pH is maintained at 4.0-6.0 by addition of acid such as HCl or H₃PO₄ during dissolution of the salt. In contrast, sodium hexametaphosphate (NaPO₃)₆ shows very high solubility and concentrated solutions (20-36%, by weight) can be prepared with no pH adjustment. The amount of phosphorylating reagent used will depend on the reagent and is selected so that the
25 resultant starch derivative contains at least 0.12% of bound phosphorus. By the term "bound phosphorus" we mean phosphorus which is attached by an ester linkage to a hydroxyl group of the anhydroglucose backbone of the derivatized starch.

Most commonly, the amount of phosphorylating reagent employed will range from 0.5 to 12% by weight of dry starch. For example, treatment of waxy maize with 3.5 to 4.0% of sodium tripolyphosphate will give a

reagent is dried to a moisture less than about 9.0% and preferably from 2.0 to 7.0% prior to the required heat reaction or roasting at higher temperatures. Ordinarily, the dry mixture of starch and phosphorylating reagent is heated to temperatures of from 110-140 °C and preferably will range from 130-135 °C during the phosphorylation reaction. The heating period may range from 0.1 to 4 hours or more depending on the
35 selected reagent, pH, temperature, etc. Care must be taken to avoid prolonged heating at higher temperatures of the starch-reagent blend during the phosphorylation reaction to avoid possible degradation of the starch. Higher temperatures and/or longer heating periods can be tolerated when the pH of the blend is within the upper portion of the designated pH range.

The starch additives of our invention may be effectively used for addition to pulp prepared from any
40 types of cellulosic fibers, synthetic fibers, or combinations. Among the cellulosic materials which may be used are bleached and unbleached sulfate (kraft), bleached and unbleached sulfite, bleached and unbleached soda, neutral sulfite, semi-chemical, chemiground wood, ground wood or any combination of these fibers. Fibers of the viscose rayon or regenerated cellulose type may also be used if desired.

Any desired inert mineral fillers may be added to the pulp which is to be modified with our improved
45 starch derivatives. Such materials include clay, titanium dioxide, talc, calcium carbonate, calcium sulfate and diatomaceous earths. Rosin may also be present, if desired.

With respect to the proportion of the starch derivative to be incorporated with the paper pulp, we have found that this may vary in accordance with the particular pulp involved. In general, we prefer to use 0.05 to 1.0% of the starch derivative, based on the dry weight of the pulp. Within this preferred range the precise
50 amount which is used will depend upon the type of pulp being used, the specific operating conditions, and the particular end-use for which the paper is intended. The use of amounts of starch derivative greater than 1%, on the dry weight of the pulp, is not precluded, but is ordinarily unnecessary in order to achieve the desired improvements. The described derivatives are used as wet-end, beater additives, although they also may be added to the pulp while the latter is in the headbox or hydropulper. When added in the proper
55 concentrations, our starch derivatives serve to increase pigment retention and paper strength, while significantly improving drainage efficiency in the papermaking process.

Thus it is seen that the starch derivatives employed in our process containing cationic and anionic groups in carefully balanced ratios and meeting other specified criteria relating to bound phosphorus and

preservation of molecular weight, yield a combination of benefits in the manufacture of paper. The wet-end additives of our invention not only provide pigment retention and strength to the paper but surprisingly provide improved drainage performance not obtainable with amphoteric starch additives of the prior art.

In the examples which follow, the bound phosphorus was determined on washed starch samples which were burned by Schöniger combustion, and the percent phosphorus was determined colorimetrically by forming molybdophosphoric complexes or determined by atomic emission spectroscopy.

All viscosity measurements of the starch derivatives were determined by a procedure using 2.0 g (db) of a washed, salt free starch sample suspended in 50 ml of distilled water. The starch and water are stirred at 260 rpm using a mechanical stirrer with a flat, stainless steel paddle (3.18 cm (1.25") in height, 3.8 cm (1.5") at the top tapered to 2.54 cm (1.0") at the bottom). While the starch mixture is stirring, 50 ml of 5.0 N KOH are added and stirring is continued for a total of 5 minutes starting with the addition of KOH. The viscosity of the dispersion is measured at room temperature within a 0.5 hours of adding the KOH, using a RVT Brookfield Viscometer employing a No. 4 spindle at 10 rpm.

Drainage performance of the various additives was carried out employing a Britt Jar modified by having an extended mixing cylinder and an agitator set at 250 rpm. Unbleached softwood Kraft is beaten to a 550 ml CSF and diluted to 0.5% consistency. Alum (3.3% by weight of the pulp) is added to the stock and the pH is adjusted to 5.5.

An amount of starch to be evaluated (1.0% db by weight of fiber), cooked for about 20 minutes, is added to a 345 ml aliquot of the pulp suspension with agitation. The suspension is then added to the Britt Jar which already contains 1,500 ml of water and the agitator is turned on. A stopper is removed from the base of the jar and the time required for 1,200 ml of water to drain through the wire screen in seconds is noted. The drainage rate is calculated in terms of ml/s. In the examples, drainage efficiency or performance is expressed as % of the control.

The following examples will further illustrate the embodiment of this invention.

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EXAMPLE I

This example illustrates the preparation of four amphoteric starch derivatives of the present invention prepared in accordance with the process of the invention. Additionally, the example illustrates the effect of phosphorylation pH on the drainage performance of the resulting starch derivative.

The following ingredients were charged into a reaction vessel fitted with means for heating and mechanical agitation:

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	Waxy maize (about 10% moisture)	7,500 g
	Water	8,250 ml

Under agitation, the slurry temperature was raised to 37°C and the pH was raised to 11.2 to 11.5 using an aqueous solution of sodium hydroxide (4% by weight). With agitation, 600 g of a 50% by weight aqueous solution of diethylaminoethylchloride HCl (DEC) were added to the slurry while maintaining the pH between 11.0 and 11.5. The latter mixture was allowed to react at 37°C for 17.5 hours. The final pH of the system was 11.3. After the reaction was completed, the pH level was adjusted to pH 7.0 with dilute (10%) hydrochloric acid and filtered. The cake was washed with 16,500 ml of water and air-dried at room temperature. It was found to have a nitrogen content of 0.33%, by weight on a dry basis (db), corresponding to a cationic D.S. (degree of substitution) of 0.038.

Six portions of this cationic starch were phosphorylated at pH levels of from 5.0 to 7.4 by the following general procedure:

Slurries were prepared by adding 1,200 g of starch to 1,500 ml of water, followed by the addition of 60 g of sodium tripolyphosphate (STP). The pH of each slurry was adjusted as indicated in Table I using 10% hydrochloric acid. The slurries were filtered and the starch filter cakes were flash dried at 82-99°C to a moisture content of 5.0 to 7.0%. Based on phosphorus analysis of the dried starches, approximately 35 g of STP were retained on the starch.

The dry-heat phosphorylation was carried out in an oil-jacketed reaction vessel equipped with a mechanical stirrer. The jacket was heated to 168-170°C. The STP-impregnated starch was added to the heated vessel, allowed to stir gently until the starch temperature reached 133°C, (approximately 13-15 minutes) and was then allowed to cool to room temperature.

The bound phosphorus, viscosity and drainage performance were determined as described above with the results summarized in Table I.

TABLE I

Sample	Adjusted pH	% Bound Phosphorus	A/C	Visc. mPa.s (cps)	Drainage Efficiency % of Control
Control*		0.10	0.173	400 (400)	100
A	5.0	0.20	0.273	400 (400)	88
B	5.5	0.20	0.273	1,400 (1,400)	121
C	6.0	0.17	0.233	1,500 (1,500)	127
D	6.5	0.17	0.233	2,400 (2,400)	126
E	7.0	0.17	0.233	2,050 (2,050)	131
F**	7.4	0.17	0.233	2,400 (2,400)	124

* The control is waxy maize containing about 0.26% cationic tertiary nitrogen (D.S. of 0.030) and about 0.10% of bound phosphorus.

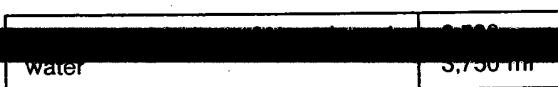
** Sample F was heated to 131 °C in 40 minutes during the phosphorylating heat reaction.

The data in the above table indicates that a pH level lower than about pH 5.5 during the phosphorylating heat reaction leads to a degradation of the amphoteric starch. Thus, Sample A which was phosphorylated at pH 5.0 shows a drainage performance which is significantly less than that of the control.

EXAMPLE II

This example illustrates the preparation and improved drainage of an amphoteric starch of the invention containing quaternary ammonium cationic groups.

The following ingredients were charged into a reaction vessel fitted with means for heating and mechanical agitation:



Under agitation, the slurry temperature was raised to 43 °C and the pH was adjusted to 11.2-11.5 using an aqueous solution of sodium hydroxide (4% by weight). With agitation, 208 g of a 60% active, aqueous solution of 3-chloro-2-hydroxypropyltrimethyl ammonium chloride were added and the mixture was allowed to react at 43 °C for 24 hours. The final pH of the system was 11.6. After the reaction was completed, the slurry was neutralized to pH 7.0 with 10% hydrochloric acid and recovered as described in Example I. The final product was found to contain 0.32% nitrogen by weight (db) corresponding to a cationic D.S. (degree of substitution) of 0.037.

About 1,000 g of the quaternary ammonium starch was slurried in 1,250 ml of water containing 40 g STP at pH 7.0. After filtering, flash-drying and heating as described in Example I, the starch was allowed to cool to room temperature. The starch contained 0.14% bound phosphorus its viscosity was 2,700 mPa.s (2,700 cps), and the A/C ratio was 0.198. Drainage performance was 129% of the control of Example I.

EXAMPLE III

In this example, a cationic starch base was phosphorylated by impregnation with the phosphorylating reagent to produce the amphoteric starch derivative of the invention.

Cationic waxy maize (1,200 g) was prepared by reaction with DEC as described in Example I except that the final slurry was neutralized to pH 8.0, filtered and not washed. A solution of STP reagent was prepared by dissolving 48 g of the salt in 126 g of water while maintaining the pH at 5.0. The solution was sprayed onto the starch filter cake, and the starch-STP blend was flash-dried and heat reacted as described in Example I. The pH of the starch-STP blend prior to heat reaction was 6.9. The blend was heated and reached a temperature of 133 °C in 9 minutes and was then allowed to cool to room temperature. The amphoteric starch contained 0.17% of bound phosphorus and its viscosity was 2,000 mPa.s (2,000 cps). The A/C ratio was 0.233. Drainage performance was 130% of the control of Example I.

EXAMPLE IV

This example illustrates the use of various starch bases and various nitrogen contents in preparing the amphoteric starch additives of this invention.

Samples of potato, tapioca and waxy maize were cationically substituted as described in Examples I or II. The phosphorylation reactions were carried out as described in Example III. The samples and test results 5 are summarized in Table II. Drainage efficiency was measured against the control of Example I.

TABLE II

Sample	Starch Base	% Bound Phosphorus	A/C	% N Tert.	% N Quat.	Visc. mPa.s (cps)	Drainage Efficiency % of Control
A	Potato	0.18	0.233	-	0.35	1,200 (1,200)	131
B	Potato	0.15	0.322	-	0.21	1,350 (1,350)	123
C	Tapioca	0.16	0.425	-	0.17	800 (800)	122
D	Tapioca	0.16	0.278	-	0.26	1,000 (1,000)	129
E	W.Maize	0.14	0.253	0.25	-	1,650 (1,650)	136
F	W.Maize	0.18	0.280	0.29	-	1,500 (1,500)	135
G*	W.Maize	0.06	0.085	0.32	-	2,300 (2,300)	100

*Sample G does not meet the bound phosphorus specification and is not within the scope of the present invention.

EXAMPLE V

This example illustrates the use of sodium hexametaphosphate as the phosphorylating reagent.

Waxy maize starch (1,200 g) was reacted with 4% DEC on the starch (db) as described in Example I. After the reaction was completed, the pH level was adjusted to pH 7.0, filtered and was used in the phosphorylating step without washing. The nitrogen content was 0.33% (db).

An aqueous solution of sodium hexametaphosphate (SODAPHOS®, supplied by FMC Corporation), was prepared by dissolving 42 g of the reagent in 100 ml of water. The phosphate solution having a pH of 7.0 was sprayed onto the cationic starch filter cake as described in Example III. The starch was heated and reached 134°C in about 7 minutes during the heat reaction. The starch contained 0.14% (db) of bound phosphorus. The A/C ratio was 0.192%. Drainage performance was 124% of the control of Example I.

EXAMPLE VI (Comparative)

This example shows the unsuitability of sodium orthophosphate as the phosphorylating reagent for preparing the starch derivatives of the present invention. The use of sodium orthophosphate to prepare amphoteric starches is described in US-A-3,562,103.

A cationic waxy maize starch containing 0.32% nitrogen by weight (db) corresponding to a cationic D.S. (degree of substitution) of 0.037, as prepared in Example II above, was used herein.

About 1,100 g of the quaternary ammonium starch was slurried in 1,200 ml of water, and 14.4 g of disodium hydrogen phosphate and 81.4 g of sodium dihydrogen phosphate were added while maintaining the pH at 5.6. The slurry was filtered and the cake dried to a moisture content of about 10%. Based on a phosphorus analysis of the dried starch, approximately 63% of the phosphorus salt was retained on the starch. The dry heat reaction of the phosphate impregnated starch was carried out in a draft oven pre-heated to 145°C keeping the starch (spread on trays) in the oven for 60, 90 and 120 minutes, samples A, B and C respectively, and cooling to room temperature.

The bound phosphorus, viscosity and drainage performance of these amphoteric starches were determined with the results summarized as follows:

Sample	Heating Time	% Bound Phosphorous	A/C	Visc. mPa.s (cps)	Drainage Efficiency % of Control
5	A	60 min.	0.09	0.127 (600) 600	83
	B	90 min.	0.16	0.226 (200) 200	82
	C	120 min.	0.18	0.254 (150) 150	90

* The control is the waxy maize control of Example I.

10 The orthophosphate reagents require longer heating and higher temperatures as compared to sodium tripolyphosphate which leads to degradation of the molecular weight (evidenced by the low viscosity of the samples) and loss of drainage performance.

Claims

15 Claims for the following Contracting States : BE, DE, FR, GB, IT, LU, NL, SE

1. A process for preparing an amphoteric starch derivative which comprises:
 - (a) providing an aqueous slurry of a starch derivative containing tertiary amino or quaternary ammonium cationic substituent groups having a degree of substitution of from 0.010 to 0.080,
 - (b) adjusting the pH level of the slurry to pH 5.5-8.5,
 - (c) adding to the aqueous starch slurry a phosphate salt selected from the group consisting of tripolyphosphate, hexametaphosphate, and pyrophosphate alkali metal salts, while maintaining the pH level at 5.5-8.5,
 - (d) filtering the slurry,
 - (e) drying the resultant cake to a moisture of 9.0 % by weight or below,
 - (f) heat reacting the dried starch at a temperature of 110-140 °C for a period of 0.1 to 4.0 hours, and
 - (g) recovering the amphoteric starch derivative, wherein the resultant starch derivative has a bound phosphorus content of at least 0.12 %, a viscosity of at least 800 mPa.s (800 cps), and a ratio of anionic to cationic groups of from 0.12 to 0.55.
2. A process for preparing an amphoteric starch derivative according to claim 1, wherein steps (c) and (f) in claim 1 have been replaced by:
 - (c) filtering the slurry to provide a starch cake containing no more than 45% of moisture,
 - (d) forming a reagent solution of an alkali metal tripolyphosphate or hexametaphosphate salt which comprises water and 20-36 % by weight of said salt,
 - (e) adding 2-30 % by weight of said reagent solution based on the weight of the starch to said starch cake to achieve efficient impregnation of the starch cake, and
 - (f) drying the resultant cake and heat reacting the dried starch-salt mixture which has a pH of 5.5 to 8.5 at a temperature of 110-140 °C for a period of 0.1 to 4.0 hours.
3. The process of claim 1 wherein in step (c) the slurry is adjusted to a pH level of 6.0-8.0, and the starch derivative of step (g) has a bound phosphorus content of at least 0.14 % and a viscosity of at least 1,000 mPa.s (1000 cps).
4. The process of claim 1, 2 or 3 wherein the starch derivative of step (a) contains tertiary amino groups and is a diethylaminoethyl ether of starch.
5. The process of claim 1, 2 or 3 wherein in step (a) the starch derivative contains quaternary ammonium groups and is a 2-hydroxypropyl trimethylammonium ether of starch.
6. The process of claim 1 or 2 wherein the starch derivative employed in step (a) is waxy maize, corn, tapioca or potato starch.
7. An amphoteric starch derivative containing tertiary amino or quaternary ammonium cationic groups and anionic phosphate groups wherein said starch derivative has a degree of substitution of cationic groups of from 0.010-0.080, a bound phosphorus content of at least 0.12 %, a viscosity of at least 800 mPa.s (800 cps), and the ratio of anionic phosphate to cationic groups is within the range of from 0.12 to 0.55.

- 8. The starch derivative of claim 7 wherein the starch is substituted with diethylaminoethyl ether groups or 2-hydroxypropyl trimethylammonium ether groups and contains a bound phosphorus content of at least 0.14 %.
- 5 9. The amphoteric starch derivative of claim 7 wherein the starch is waxy maize, corn, tapioca or potato starch.
- 10 10. In a process for making paper, the step which comprises adding to the stock prior to passing the stock onto the wire screen, a starch derivative according to claim 7.

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Claims for the following Contracting States : AT, ES

- 1. A process for preparing an amphoteric starch derivative which comprises:
 - 15 (a) providing an aqueous slurry of a starch derivative containing tertiary amino or quaternary ammonium cationic substituent groups having a degree of substitution of from 0.010 to 0.080,
 - (b) adjusting the pH level of the slurry to pH 5.5-8.5,
 - (c) adding to the aqueous starch slurry a phosphate salt selected from the group consisting of tripolyphosphate, hexametaphosphate, and pyrophosphate alkali metal salts, while maintaining the pH level at 5.5-8.5,
 - 20 (d) filtering the slurry,
 - (e) drying the resultant cake to a moisture of 9.0 % by weight or below,
 - (f) heat reacting the dried starch at a temperature of 110-140 °C for a period of 0.1 to 4.0 hours, and
 - (g) recovering the amphoteric starch derivative, wherein the resultant starch derivative has a bound phosphorus content of at least 0.12 %, a viscosity of at least 800 mPa.s (800 cps), and a ratio of anionic to cationic groups of from 0.12 to 0.55.
- 25 2. A process for preparing an amphoteric starch derivative according to claim 1 wherein steps (c), (d), (e) and (f) in claim 1 have been replaced by:
 - 30 (c) filtering the slurry to provide a starch cake containing no more than 45 % of moisture,
 - (d) forming a reagent solution of an alkali metal tripolyphosphate or hexametaphosphate salt which comprises water and 20-36 % by weight of said salt,
 - (e) adding 2-30 % by weight of said reagent solution based on the weight of the starch to said starch cake to achieve efficient impregnation of the starch cake, and
 - 35 (f) drying the resultant cake and heat reacting the dried starch-salt mixture which has a pH of 5.5 to 8.5 at a temperature of 110-140 °C for a period of 0.1 to 4.0 hours.
- 40 3. The process of claim 1 wherein in step (c) the slurry is adjusted to a pH level of 6.0-8.0, and the starch derivative of step (g) has a bound phosphorus content of at least 0.14 % and a viscosity of at least 1,000 mPa.s (1000 cps).
- 45 4. The process of claim 1, 2 or 3 wherein the starch derivative of step (a) contains tertiary amino groups and is a diethylaminoethyl ether of starch.
- 5. The process of claim 1, 2 or 3 wherein in step (a) the starch derivative contains quaternary ammonium groups and is a 2-hydroxypropyl trimethylammonium ether of starch.
- 6. The process of claim 1 or 2 wherein the starch derivative employed in step (a) is waxy maize, corn, tapioca or potato starch.
- 50 7. In a process for making paper the step which comprises adding to the stock prior to passing the stock onto the wire screen an amphoteric starch derivative containing tertiary amino or quaternary ammonium cationic groups and anionic phosphate groups wherein said starch derivative has a degree of substitution of cationic groups of from 0.010-0.080, a bound phosphorus content of at least 0.12 %, a viscosity of at least 800 mPa.s (800 cps), and the ratio of anionic phosphate to cationic groups is within the range of from 0.12 to 0.55.
- 55 8. In a process of claim 7 wherein the starch is substituted with diethylaminoethyl ether groups or 2-hydroxypropyl trimethylammonium ether groups and contains a bound phosphorus content of at least

0.14 %.

9. In a process of claim 7 wherein the starch is waxy maize, corn, tapioca or potato starch.

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Revendications pour les Etats contractants suivants : BE, DE, FR, GB, IT, LU, NL, SE

1. Procédé de préparation d'un dérivé d'amidon amphotère, qui consiste :
 - (a) à préparer une suspension aqueuse d'un dérivé d'amidon contenant des groupes cationiques amino tertiaire ou ammonium quaternaire de substitution, ayant un degré de substitution de 0,010 à 0,080,
 - (b) à ajuster le pH de la suspension à une valeur de 5,5 à 8,5,
 - (c) à ajouter à la suspension aqueuse d'amidon un phosphate choisi dans le groupe comprenant des tripolyphosphates, des hexamétaphosphates et des pyrophosphates de métaux alcalins, tout en maintenant le pH à une valeur de 5,5 à 8,5,
 - (d) à filtrer la suspension,
 - (e) à sécher le gâteau résultant à une teneur en humidité égale ou inférieure à 9,0% en poids,
 - (f) à soumettre l'amidon séché à une réaction à chaud à une température de 110 à 140 °C pendant un temps de 0,1 à 4,0 heures, et
 - (g) à recueillir le dérivé d'amidon amphotère, le dérivé d'amidon résultant ayant une teneur en phosphore lié d'au moins 0,12%, une viscosité d'au moins 800 mPa.s (800 cps) et un rapport des groupes anioniques aux groupes cationiques de 0,12 à 0,55.
2. Procédé de préparation d'un dérivé d'amidon amphotère suivant la revendication 1, dans lequel les étapes (c), (d), (e) et (f) dans la revendication 1 ont été remplacées par les étapes suivantes :
 - (c) filtration de la suspension pour obtenir un gâteau d'amidon ne contenant pas plus de 45% d'humidité,
 - (d) formation d'une solution réactive d'un tripolyphosphate ou hexamétaphosphate de métal alcalin comprenant de l'eau et 20 à 36% en poids dudit sel.

gâteau d'amidon pour parvenir à une imprégnation efficace du gâteau d'amidon, et
 (f) séchage du gâteau résultant et réaction à chaud du mélange amidon-sel séché qui possède un pH de 5,5 à 8,5 à une température de 110 à 140 °C pendant un temps de 0,1 à 4,0 heures.

- 35 3. Procédé suivant la revendication 1, dans lequel, dans l'étape (c), la suspension est ajustée à un pH de 6,0 à 8,0 et le dérivé d'amidon de l'étape (g) possède une teneur en phosphore lié d'au moins 0,14% et une viscosité d'au moins 1000 mPa.s (1000 cps).
- 40 4. Procédé suivant la revendication 1, 2 ou 3, dans lequel le dérivé d'amidon de l'étape (a) contient des groupes amino tertiaire et est un éther diéthylaminoéthylique d'amidon.
5. Procédé suivant la revendication 1, 2 ou 3, dans lequel, dans l'étape (a), le dérivé d'amidon contient des groupes ammonium quaternaire et est un éther de 2-hydroxypropyl-triméthylammonium d'amidon.
- 45 6. Procédé suivant la revendication 1 ou 2, dans lequel le dérivé d'amidon utilisé dans l'étape (a) est l'amidon de mais cireux, l'amidon de mais, la féculle de manioc ou la féculle de pomme de terre.
7. Dérivé d'amidon amphotère contenant des groupes cationiques amino tertiaire ou ammonium quaternaire et des groupes anioniques phosphate, ledit dérivé d'amidon possédant un degré de substitution par des groupes cationiques de 0,010 à 0,080, une teneur en phosphore lié d'au moins 0,12%, une viscosité d'au moins 800 mPa.s (800 cps), le rapport des groupes phosphate anioniques aux groupes cationiques étant compris dans l'intervalle de 0,12 à 0,55.
- 50 8. Dérivé d'amidon suivant la revendication 7, dans lequel l'amidon est substitué avec des groupes éther diéthylaminoéthylique ou des groupes éther de 2-hydroxypropyl-triméthylammonium et possède une teneur en phosphore lié d'au moins 0,14%.
9. Dérivé d'amidon amphotère suivant la revendication 7, dans lequel l'amidon est l'amidon de mais

cireux, l'amidon de mais, la férule de manioc ou la férule de pomme de terre.

10. Procédé de production de papier, dans lequel une étape consiste à ajouter à la pâte à papier, avant le passage de la pâte à papier sur le tamis en toile métallique, un dérivé d'amidon suivant la revendication 7.

Revendications pour les Etats contractants suivants : AT, ES

1. Procédé de préparation d'un dérivé d'amidon amphotère, qui consiste :
 - (a) à préparer une suspension aqueuse d'un dérivé d'amidon contenant des groupes cationiques amino tertiaire ou ammonium quaternaire de substitution, ayant un degré de substitution de 0,010 à 0,080,
 - (b) à ajuster le pH de la suspension à une valeur de 5,5 à 8,5,
 - (c) à ajouter à la suspension aqueuse d'amidon un phosphate choisi dans le groupe comprenant des tripolyphosphates, des hexamétaphosphates et des pyrophosphates de métaux alcalins, avec maintien du pH à une valeur de 5,5 à 8,5,
 - (d) à filtrer la suspension,
 - (e) à sécher le gâteau résultant à une teneur en humidité égale ou inférieure à 9,0% en poids,
 - (f) à soumettre l'amidon séché à une réaction à chaud à une température de 110 à 140 °C pendant un temps de 0,1 à 4,0 heures, et
 - (g) à recueillir le dérivé d'amidon amphotère, le dérivé d'amidon résultant possédant une teneur en phosphore lié d'au moins 0,12%, une viscosité d'au moins 800 mPa.s (800 cps) et un rapport des groupes anioniques aux groupes cationiques de 0,12 à 0,55.
2. Procédé de préparation d'un dérivé d'amidon amphotère suivant la revendication 1, dans lequel les étapes (c), (d), (e) et (f) dans la revendication 1 ont été remplacées par les étapes suivantes :
 - (c) filtration de la suspension pour obtenir un gâteau d'amidon ne contenant pas plus de 45% d'humidité,
 - (d) formation d'une solution réactive d'un tripolyphosphate ou hexamétaphosphate de métal alcalin qui comprend de l'eau et 20 à 36% en poids dudit sel,
 - (e) addition de 2 à 30% en poids de ladite solution réactive, sur la base du poids de l'amidon, audit gâteau d'amidon pour parvenir à une imprégnation efficace du gâteau d'amidon, et
 - (f) séchage du gâteau résultant et réaction à chaud du mélange amidon-sel séché, qui possède un pH de 5,5 à 8,5, à une température de 110 à 140 °C pendant un temps de 0,1 à 4,0 heures.
3. Procédé suivant la revendication 1, dans lequel, dans l'étape (c), la suspension est ajustée à un pH de 6,0 à 8,0 et le dérivé d'amidon de l'étape (g) possède une teneur en phosphore lié d'au moins 0,14% et une viscosité d'au moins 1000 mPa.s (1000 cps).
4. Procédé suivant la revendication 1, 2 ou 3, dans lequel le dérivé d'amidon de l'étape (a) contient des groupes amino tertiaire et est un éther diéthylaminoéthylique d'amidon.
5. Procédé suivant la revendication 1, 2 ou 3, dans lequel, dans l'étape (a), le dérivé d'amidon contient des groupes ammonium quaternaire et est un éther de 2-hydroxypropyl-triméthylammonium d'amidon.
6. Procédé suivant la revendication 1 ou 2, dans lequel le dérivé d'amidon utilisé dans l'étape (a) est l'amidon de mais cireux, l'amidon de mais, la férule de manioc ou la férule de pomme de terre.
7. Procédé de production de papier, dans lequel une étape consiste à ajouter à la pâte à papier avant le passage de la pâte à papier sur le tamis en toile métallique, un dérivé d'amidon amphotère contenant des groupes cationiques amino tertiaire ou ammonium quaternaire et des groupes anioniques phosphate, ledit dérivé d'amidon possédant un degré de substitution avec des groupes cationiques de 0,010 à 0,080, une teneur en phosphore lié d'au moins 0,12%, une viscosité d'au moins 800 mPa.s (800 cps), et un rapport des groupes anioniques phosphate aux groupes cationiques compris dans l'intervalle de 0,12 à 0,55.
8. Procédé suivant la revendication 7, dans lequel l'amidon est substitué avec des groupes éther de diéthylamino-éthyle ou des groupes éther de 2-hydroxypropyl-triméthylammonium et possède une

teneur en phosphore lié d'au moins 0,14%.

9. Procédé suivant la revendication 7, dans lequel l'amidon est l'amidon de maïs cireux, l'amidon de maïs, la féculle de manioc ou la féculle de pomme de terre.

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Patentansprüche

Patentansprüche für folgende Vertragsstaaten : BE, DE, FR, GB, IT, LU, NL, SE

1. Verfahren zur Herstellung eines amphoteren Stärkederivates, das umfaßt:
 - (a) die Bereitstellung einer wäßrigen Aufschämmung eines Stärkederivates, das kationische tertiäre Amino- oder quaternäre Ammoniumsubstituentengruppen mit einem Substitutionsgrad von 0,010 bis 0,080 enthält,
 - (b) die Einstellung des pH-Wertes der Aufschämmung auf 5,5 bis 8,5,
 - (c) die Zugabe eines Phosphatsalzes, ausgewählt aus der aus Tripolyphosphat-, Hexametaphosphat- und Pyrophosphatkaliimetallsalzen bestehenden Gruppe, zur wäßrigen Stärkeaufschämmung, wobei der pH-Wert auf 5,5 bis 8,5 gehalten wird.
 - (d) das Filtrieren der Aufschämmung,
 - (e) das Trocknen des erhaltenen Kuchens auf eine Feuchtigkeit von 9,0 Gew.-% oder weniger,
 - (f) die Wärmereaktion der getrockneten Stärke bei einer Temperatur von 110 bis 140 °C für eine Dauer von 0,1 bis 4,0 h und
 - (g) die Gewinnung des amphoteren Stärkederivates, wobei das erhaltene Stärkederivat einen Gehalt an gebundenem Phosphor von mindestens 0,12 %, eine Viskosität von mindestens 800 mPa.s (800 cps) und ein Verhältnis von anionischen zu kationischen Gruppen von 0,12 bis 0,55 aufweist.

2. Verfahren zur Herstellung eines amphoteren Stärkederivates gemäß Anspruch 1, worin die Schritte (c), (d), (e) und (f) in Anspruch 1 durch:
 - (c) das Filtrieren der Aufschämmung zur Bildung eines Stärkekuchens, der nicht mehr als 45 % Feuchtigkeit enthält,
 - (d) die Bildung einer Reagenzlösung eines Alkalimetalltripolyphosphat- oder
 - (e) die Zugabe von 2 bis 30 Gew.-% der Reagenzlösung, bezogen auf das Gewicht der Stärke, zu dem Stärkekuchen, um eine wirksame Imprägnierung desselben zu erreichen, und
 - (f) das Trocknen des erhaltenen Kuchens und die Wärmereaktion der getrockneten Stärke-Salz-Mischung, die einen pH-Wert von 5,5 bis 8,5 hat, bei einer Temperatur von 110 bis 140 °C für eine Dauer von 0,1 bis 4,0 h,

ersetzt worden sind.

3. Verfahren gemäß Anspruch 1, worin in Schritt (c) die Aufschämmung auf einen pH-Wert von 6,0 bis 8,0 eingestellt wird und das Stärkederivat von Schritt (g) einen Gehalt an gebundenem Phosphor von mindestens 0,14 % und eine Viskosität von mindestens 1 000 mPa.s (1000 cps) hat.

4. Verfahren gemäß Anspruch 1, 2 oder 3, worin das Stärkederivat von Schritt (a) tertiäre Aminogruppen enthält und ein Diethylaminoethylether von Stärke ist.

- 45 5. Verfahren gemäß Anspruch 1, 2 oder 3, worin in Schritt (a) das Stärkederivat quaternäre Ammoniumgruppen enthält und ein 2-Hydroxypropyltrimethylammoniumether von Stärke ist.

6. Verfahren gemäß Anspruch 1 oder 2, worin das in Schritt (a) verwendete Stärkederivat eine Wachsmais-, Mais-, Tapioka- oder Kartoffelstärke ist.

- 50 7. Amphoteres Stärkederivat, das kationische tertiäre Amino- oder quaternäre Ammoniumgruppen und anionische Phosphatgruppen enthält, worin das Stärkederivat einen Substitutionsgrad von kationischen Gruppen von 0,010 bis 0,080, einen Gehalt an gebundenem Phosphor von mindestens 0,12 %, eine Viskosität von mindestens 800 mPa.s (800 cps) aufweist und das Verhältnis von anionischen Phosphatgruppen zu kationischen Gruppen im Bereich von 0,12 bis 0,55 liegt.

8. Stärkederivat gemäß Anspruch 7, worin die Stärke mit Diethylaminoethylethergruppen oder 2-Hydroxypropyltrimethylammoniumethergruppen substituiert ist und einen Gehalt an gebundenem Phosphor

von mindestens 0,14 % aufweist.

9. Amphoteres Stärkederivat nach Anspruch 7, worin die Stärke Wachsmais-, Mais-, Tapioka- oder Kartoffelstärke ist.
- 5 10. In einem Verfahren zur Papierherstellung die Stufe, die die Zugabe eines Stärkederivates gemäß Anspruch 7 zu dem Papierstoff vor dessen Beförderung auf das Drahtsieb umfaßt.

Patentansprüche für folgende Vertragsstaaten : AT, ES

10. 1. Verfahren zur Herstellung eines amphoteren Stärkederivates, das umfaßt:
 - (a) die Bereitstellung einer wäßrigen Aufschlämmung eines Stärkederivates, das kationische tertiäre Amino- oder quaternäre Ammoniumsubstituentengruppen mit einem Substitutionsgrad von 0,010 bis 0,080 enthält,
 - (b) die Einstellung des pH-Wertes der Aufschlämmung auf 5,5 bis 8,5,
 - (c) die Zugabe eines Phosphatsalzes, ausgewählt aus der aus Tripolyphosphat-, Hexametaphosphat- und Pyrophosphatkaliimetallsalzen bestehenden Gruppe, zur wäßrigen Stärkeaufschlämmung, wobei der pH-Wert auf 5,5 bis 8,5 gehalten wird,
 - (d) das Filtrieren der Aufschlämmung,
 - (e) das Trocknen des erhaltenen Kuchens auf eine Feuchtigkeit von 9,0 Gew.-% oder weniger,
 - (f) die Wärmereaktion der getrockneten Stärke bei einer Temperatur von 110 bis 140 °C für eine Dauer von 0,1 bis 4,0 h und
 - (g) die Gewinnung des amphoteren Stärkederivates, wobei das erhaltene Stärkederivat einen Gehalt an gebundenem Phosphor von mindestens 0,12 %, eine Viskosität von mindestens 800 mPa.s (800 cps) und ein Verhältnis von anionischen zu kationischen Gruppen von 0,12 bis 0,55 aufweist.
20. 2. Verfahren zur Herstellung eines amphoteren Stärkederivates gemäß Anspruch 1, worin die Schritte (c), (d), (e) und (f) in Anspruch 1 durch:
 - (c) das Filtrieren der Aufschlämmung zur Bildung eines Stärkekuchens, der nicht mehr als 45 % Feuchtigkeit enthält,
 - (d) die Bildung einer Reagenzlösung eines Alkalimetalltripolyphosphat- oder hexametaphosphatsalzes, die Wasser und 20 bis 35 Gew.-% des Salzes umfaßt,
 - (e) die Zugabe von 2 bis 30 Gew.-% der Reagenzlösung, bezogen auf das Gewicht der Stärke, zu dem Stärkekuchen, um eine wirksame Imprägnierung desselben zu erreichen, und
 - (f) das Trocknen des erhaltenen Kuchens und die Wärmereaktion der getrockneten Stärke-Salz-Mischung, die einen pH-Wert von 5,5 bis 8,5 hat, bei einer Temperatur von 110 bis 140 °C für eine Dauer von 0,1 bis 4,0 h, ersetzt worden sind.
30. 3. Verfahren gemäß Anspruch 1, worin in Schritt (c) die Aufschlämmung auf einen pH-Wert von 6,0 bis 8,0 eingestellt wird und das Stärkederivat von Schritt (g) einen Gehalt an gebundenem Phosphor von mindestens 0,14 % und eine Viskosität von mindestens 1 000 mPa.s (1000 cps) hat.
40. 4. Verfahren gemäß Anspruch 1, 2 oder 3, worin das Stärkederivat von Schritt (a) tertiäre Aminogruppen enthält und ein Diethylaminoethylether von Stärke ist.
45. 5. Verfahren gemäß Anspruch 1, 2 oder 3, worin in Schritt (a) das Stärkederivat quaternäre Ammoniumgruppen enthält und ein 2-Hydroxypropyltrimethylammoniumether von Stärke ist.
50. 6. Verfahren gemäß Anspruch 1 oder 2, worin das in Schritt (a) verwendete Stärkederivat eine Wachsmais-, Mais-, Tapioka- oder Kartoffelstärke ist.
55. 7. In einem Verfahren zur Papierherstellung die Stufe, die die Zugabe eines amphoteren Stärkederivates zu dem Papierstoff vor dessen Beförderung auf das Drahtsieb umfaßt, wobei das amphotere Stärkederivat kationische tertiäre Amino- oder quaternäre Ammoniumgruppen und anionische Phosphatgruppen enthält, und einen Substitutionsgrad von kationischen Gruppen von 0,010 bis 0,080, einen Gehalt an gebundenem Phosphor von mindestens 0,12 %, eine Viskosität von mindestens 800 mPa.s (800 cps) aufweist und das Verhältnis von anionischen Phosphatgruppen zu kationischen Gruppen im Bereich von

0,12 bis 0,55 liegt.

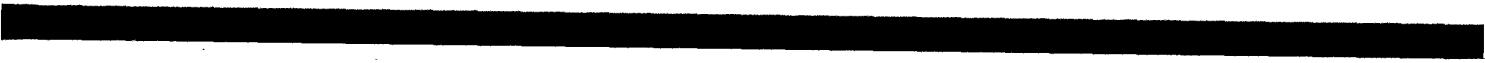
8. Verfahren gemäß Anspruch 7, worin die Stärke mit Diethylaminoethylethergruppen oder 2-Hydroxypropyltrimethylammoniumethergruppen substituiert ist und einen Gehalt an gebundenem Phosphor von mindestens 0,14 % aufweist.
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9. Verfahren gemäß Anspruch 7, worin die Stärke Wachsmais-, Mais-, Tapioka- oder Kartoffelstärke ist.

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